

LAUNCH **OPERATIONS** CENTER

July 15, 1963 OTS:

N64-16706

Cocle 1

160776 John F. Kennedy Space (NASA TMX5-4645;
Center, Cocoa Blach, Fla.

SPECIALIZED COST STUDY,

LAUNCH COMPLEX 39-

PNEUMATIC SYSTEM

M. B. Loeb 15 Jul, 1963 23 p refs

OTS PRICE

XEROX \$ 2.60-0K MICROFILM \$.89 MJ

LAUNCH OPERATIONS CENTER

TR-4-13-2-D

SPECIALIZED COST STUDY, LAUNCH COMPLEX 39-PNEUMATIC SYSTEM

by M. B. Loeb

ABSTRACT

16706

A

This report presents the results of a specialized cost study upon which the decisions affecting design responsibilities of the LO-DP23 office concerning the conversion, compression, transmission, and high-pressure storage portions of the pneumatic system for Launch Complex 39 can be based.

The report covers cost responsibilities of the LO-DP23 office concerning pneumatic systems for conversion, transmission, and storage of gases at various pressures from 6000 psig to 10,000 psig. The report shows that the optimum conditions of design occur at 12,000, 10,000, and 7,400 psig, depending on the selection of materials used for the cross-country pipe. These optimum pressures are for systems with cross-country pipe materials of AISI 4320 steel with stainless liner, Al06 Gr. C steel pipe with stainless liner, and type 316 stainless steel, respectively. These were the only pipe materials considered.

NUTHOR

LAUNCH	OPERATIONS	CENTER
	TR-4-13-2-D	

SPECIALIZED COST STUDY LAUNCH COMPLEX 39 PNEUMATIC SYSTEM

by

M. B. Loeb

Prepared by:

PROPELLANT SYSTEMS BRANCH
LAUNCH SUPPORT EQUIPMENT ENGINEERING DIVISION

TABLE OF CONTENTS

Introduction	Page	No 1
Description	,	3
Converters and Gompressors	,	3
Converter-Compressor Facility Interconnecting Piping	•	3
Cross-country Transmission Piping	•	4
High-Pressure Storage Battery	•	5
Overall Costs	•	5
Conclusions	•	6
Recommendations	•	7
Appendix		8

LIST OF ILLUSTRATIONS

Number	<u>Title</u>
Fig. 1	Composite Cost Chart, Pneumatic Systems, Cost Comparisons
Fig. 2	Nitrogen Pipe Line I.D. Variations with Pressure
Fig. 3	Nitrogen Pipe Wall Thickness Variations with Pressure
Fig. 4	Helium Pipe Line I.D. Variations with Pressure
Fig. 5	Helium Pipe Wall Thickness Variations with Pressure
Fig. 6	Storage Vessel Costs
Fig. 7	Optimum Storage Pressure
Fig. 8	Optimum Storage Pressure
Fig. 9	Comparison Costs

DEFINITION OF TERMS

Converter: Mechanical pumping and vaporizing equipment used to convert liquid nitrogen to high-pressure gaseous nitrogen.

Compressor and Converter Interconnecting Piping: Includes all low-pressure type 316 stainless steel induction piping from the liquid nitrogen and gaseous helium storage to the converters and compressors; and the type 316 stainless steel high-pressure discharge piping from the converters and the compressors to the cross-country transmission piping.

Cross-country Transmission Piping: Piping used to transport high-pressure gaseous nitrogen and helium from the converter-compressor facility to the high-pressure battery storage facilities at the launch pads and the Vertical Assembly building.

<u>Design Pressure</u>: The system working pressure of the storage battery vessels.

Residual Storage Pressure: The lowest pressure of the storage battery vessels during a launch operation.

Operating Pressure: Any storage battery vessel pressure between design and residual pressure.

Water Volume Storage: The fixed vessel volume in cubic feet.

<u>Unit Vessel Costs</u>: The cost per cubic foot water volume of fabricated storage vessel.

Battery Interconnecting Piping and Manifolding: Includes all high-pressure piping from the cross-country transmission pipe systems interface to the storage battery vessels, the interconnecting piping and manifolding of the high-pressure gaseous nitrogen storage vessels and the high-pressure gaseous helium vessels, and the discharge piping from the nitrogen and helium storage vessels to the ground level interface at the Launcher Umbilical Transporter.

<u>Primary Pressure Regulation System</u>: The primary pressure regulation system, as it now exists, is connected between the high pressure gaseous helium and nitrogen ground interface at the LUT and the control panels on the LUT.

INTRODUCTION

The factors to be considered in the design of the pneumatic system for Launch Complex 39 are: availability of operating equipment, selection of materials, reliability, and the costs involved. Within the limits of operating possibilities, selection of available materials, available operating equipment, and other design variations, there are numerous possible designs. To establish a basis for sound economical design, within the assigned responsibility of LO-DP23, the various costs involved within the allowable limits of design were considered and the results tabulated for comparison. The primary pressure regulation of the pneumatic system has become the responsibility of LO-DP23 as a result of group meetings between LO-DP23 and LO-DE23 held during the preparation of this report.

The system was categorized as follows:

- a. Converters and compressors
- b. Converter/compressor interconnecting piping
- c. Cross-country transmission piping
- d. Battery storage vessels
- e. Battery interconnecting piping
- f. Primary pressure regulation

The pneumatic system consists of two separate gas handling systems: one for nitrogen, and one for helium. The nitrogen gas system requires pumps and vaporizers to convert liquid nitrogen to high-pressure gaseous nitrogen. The helium gas system requires the use of mechanical compression equipment to raise the pressure of gaseous helium from tube tank cars to the battery storage pressure.

In this report the variables of the above systems are considered separately at six incremental pressure steps. The resulting cost variations of each part of the system are charted. To establish overall costs, the costs of the individual parts of the system are combined.

The technical requirements of design and cost of electrical sub-station and power distribution, buildings and superstructures, concrete foundations and supports, specialized instrumentation, and the associated pneumatic systems operating at less than 6,000 psig are not considered in this report.

The costs are based on LO-DP23 estimates, manufacturers' surveys, and system cost comparisons. These estimates yield a high degree of accuracy for reviewing design decisions of cost differences specific to LO-DP23 responsibilities. The data furnished relate costs to specific specialized mechanical responsibilities of the LO-DP23 office and are intended to be informative for LO-DP23 review and review by others interested in this specialized design area.

DESCRIPTION

1. Converters and Compressors. The nitrogen converters are obtainable commercially as standard, complete, self-contained units capable of delivering 1,100 standard cubic feet per minute at 6,000 psig. The helium compressors are also standard, complete, self-contained commercial units that are capable of delivering 150 standard cubic feet per minute of helium at 6,000 psig. Both units will deliver gas from 6,000 to 10,000 psig. The efficiency of these units decreases as the discharge pressure requirements increases. The design flow rate of these units, as mentioned, in a minimum value considered constant within the discharge pressure range from 6,000 to 10,000 psig for design purposes. No allowance is provided for changes in capacity resulting from changes in efficiencies.

In each sub-system, the converters and compressors perform two functions: they furnish the initial pressurization of the storage battery vessels, and they replenish the vessels during operation to maintain operating pressure during peak demands. In this report, the replenish rate determines the number of converters and compressors. The replenish rate requirement in standard cubic feet per minute is independent of pressure and is constant regardless of the pneumatic system design pressure. Therefore, the same basic number of compressor units and converter units are required regardless of the system design pressure.

Based on the replenish rate required, four operating helium compressors and one spare totalling \$140,000, and five operating liquid nitrogen converters and one spare totalling \$400,000 are required. The total cost is \$540,000. (See figure 1, column 7.)

2. Converter-compressor Facility Interconnecting Piping.
Piping for the converter-compressor facility consists of low-pressure type 316 stainless steel induction piping and high-pressure type 316 stainless steel discharge piping. The greater portion of the piping in this area is low-pressure induction piping. The induction piping design remains the same regardless of the high-pressure gas system design pressure. The high-pressure discharge piping designed for 6,000 psig with 4/1 safety factor based on ultimate strength is also suitable for pressures to 7,500 psig with 3/1 safety factor based on ultimate strength. Discharge piping designed for 8,000 psig is also suitable for pressures to 10,000 psig. It is estimated that the cost increase in the discharge piping system for pressures above 7,500 psig is \$12,500. The estimated costs of the converter-compressor facility piping are shown in figure 1, column 8.

- 3. <u>Cross-country Transmission Piping</u>. Based on environmental conditions, pressures, cleanliness levels, availability, material costs, installation requirements, and other system requirements, three materials for the cross-country piping were considered, and their costs estimated. These materials and assumptions made are:
- a. AISI 4320 steel pipe with stainless liner, 3:1 safety factor based on ultimate strength of 93,950 psi (2:1 on yield).
- b. A106 Grade C steel pipe with stainless liner, 3.5:1 safety factor based on ultimate strength of 70,000 psi. A106, Grade C steel conforms to ASTM Specification A-106-61T. (2:1 on yield).
- c. Type 316 stainless steel pipe, 3.5:1 safety factor based on ultimate strength of 74,900 psi. This piping material conforms to ASTM Specification A-312-61T (2:1 on yield)

The following additional assumptions were made:

- a. The pressure drop in the cross-country piping system will not exceed 10 percent of the converter-compressor facility delivery pressure at the most remote part of the system while delivering the unrestricted full replenish rate.
- b. The most remote part of the cross-country piping system, for pressure drop calculation purposes, is the Pad C storage battery interface.
- c. One inside diameter requirement for the piping can be selected which can meet the capacity requirements as a minimum delivery guarantee. All design pressures within the range of 6,000 to 10,000 psig will deliver full unrestricted replenish rate or more with 10 percent or less pressure drop within the system.

The determination of inside diameter requirements for the cross-country lines is presented in chart form. (See figure 2 for GN₂ system and figure 4 for GHe system.)

Pipe inside diameter requirements were determined to be 2-1/2 inches for nitrogen piping system and 1 inch for helium piping system. Based on these sizes, the wall thickness requirements were determined at various design pressures from 6,000 psi to 10,000 psi. The wall thicknesses are shown in figures 3 and 5. Using inside diameter and wall thickness data, unit prices were obtained corresponding to the various system design pressures. The lengths of pipe and total piping system costs at specific pressures and with the three materials are shown in figure 1, columns 12, 13, 14 and 15.

4. <u>High-Pressure Storage Battery</u>. The Propellant Systems Branch has made a survey of pressure vessel costs per cubic foot of water volume as related to vessel design pressure. Results of this survey are shown in figure 6. Selected unit costs based on the chart in figure 6 are shown in figure 1, column 3.

A minimum, or residual, pressure of 4,000 psig remains in the battery after use. This residual pressure is correlated with design pressure, volumetric storage efficiency, and unit costs in determining optimum storage battery pressure. (See figure 7). The effect of design pressure on storage efficiency can be compared in figure 1, columns 1 and 2. Total vessel costs can be obtained from the volume requirements and the vessel unit costs. (See figure 1, column 4.)

The costs of the interconnecting battery piping at six pressures were prepared from suppliers' prices and office estimates. The results are shown in figure 1, column 6.

5. Overall Costs. The overall costs for Pad A at the six assumed pressures are shown in figure 1, column 16. These costs are shown for each of the three materials considered for the cross-country piping. Overall costs for Pads B and C and the VAB are shown in figure 1, columns 17, 18 and 19, respectively. The cost for Pad A includes the converter-compressor facility. Cost of the converter-compressor facility is not included in the total cost of Pads B, C, and the VAB pneumatic system, because one converter-compressor facility supplies all pads and the VAB.

The total system cost for all three pads and the VAB combined is shown in figure 1, column 20.

The optimum design pressure in relation to total costs for each cross-country line material is shown graphically in figure 9.

CONCLUSTONS

- 1. The lowest costs for the system result when pneumatic system design pressures are 12,000 psig, 10,000 psig, and 7,400 psig, using 4320 steel, A-106 steel, and type 316 stainless steel, respectively, as cross-country pipe line material. (See figure 9)
- 2. The lowest costs for storage vessels result with a design storage pressure of 9,700 psig for gaseous nitrogen and 11,500 psig for gaseous helium. (See figure 7).
- 3. Costs of the following decrease with increase in design pressure:
 - a. Total storage vessel battery (see figure 1, column 4).
- b. Battery interconnecting piping and manifolding (see figure 1, column 6).
- 4. The cost of converter and compressor equipment remains constant regardless of pressure within the range of 6,000 to 10,000 psig (See figure 1, column 7).
- 5. The cost of cross-country pipe lines increases with increases in design pressure (see figure 1, columns 12, 13, 14 and 15).
- 6. The volumetric storage efficiency of the storage battery increases with increases in design pressure, resulting in lowered battery costs and smaller required storage area at higher pressures (see figure 1, column 5).

RECOMMENDATIONS

- 1. It is recommended that the existing high-pressure (7,500 to 10,000 psig) test and evaluation programs be continued so that high-pressure pneumatic systems can be designed to realize the cost savings possible at the higher pressures. This program is expected to furnish the necessary information on pressure regulators, and AISI 4320 steel for field constructed pipe lines.
- 2. It is recommended that ASTM A-106-61T, Grade C steel pipe, mechanically coupled, with a Series 300 steel liner, be used in the design of Launch Complex 39 cross-country piping. A system design pressure of 7,500 psig is recommended to realize cost savings when the programs of paragraph number one are satisfactorily concluded. This recommendation is contingent upon scheduling which affects cost.
- 3. It is recommended that the operating pressure of the LC 39 pneumatic system be 6,000 psig until the test programs are satisfactorily concluded.
- 4. It is recommended that the primary pressure regulation equipment be physically located between the storage battery and the ground level interface at the Launcher/Umbilical Transporter.

APPENDIX

Various manufacturers and governmental agencies which operate high pressure systems were contacted to determine the existence and reliability of various operating equipment within the range of 6,000 and 10,000 pounds per square inch. A sampling of the various organizations contacted are listed below. The number appearing in parentheses represents the operating pressures in pounds per square inch gage being used by them in continuous service duty.

- 1. Hercules Powder Company (15,000) Louisiana, Missouri gaseous nitrogen and hydrogen service.
- 2. DuPont de Nemours and Co. (15,000) Belle, West Virginia gaseous nitrogen and hydrogen service.
- 3. Mississippi Chemical Company (15,000) Yazoo City, Mississippi gaseous nitrogen and hydrogen service.
- 4. W. R. Grace Company (12,500) Memphis, Tennessee gaseous nitrogen and hydrogen service.
- 5. Cooperative Farm Chemical Association (12,000) Lawrence, Kansas gaseous nitrogen and hydrogen service.
- 6. John Deere (12,000) Pryor, Oklahoma gaseous nitrogen and hydrogen service.
- 7. Big Three Welding Company (7,500) Houston, Texas liquid and gaseous nitrogen.
- 8. Nitro-Well Incorporated (7,500 and 10,000) liquid and gaseous nitrogen.

This list is for reference purposes only and does not include all known systems.

From the above references it has been determined that systems and component parts of systems are presently being manufactured and used in comparable systems to the systems represented in this report.

The following technical publications were used as basic reference material:

1. "Saturn C-5 Pneumatics Handling Preliminary Criteria" ER13561 dated August 1, 1962, Contract NAS10-33 by Beech Aircraft Corporation, Boulder Division, P. O. Box 631, Boulder, Colorado.

2. "A compendium of the Properties of Materials at Low Temperature" (Phase I and II).

WADD Technical Report 60-58 by Aeronautical Systems Division, Air Force Systems Command, United States Air Force, Wright-Patterson Air Force Base, Ohio.

- 3. "Design Handbook for Liquid and Gaseous Helium Handling Equipment". ASD Technical Report 61-226 Aeronautical Systems Division, Air Force Systems Command, United States Air Force, Wright-Patterson Air Force Base, Ohio.
- 4. "Physical and Thermodynamics Properties of Helium" by Whittaker Controls Division of Telecomputing Corporation 1957.
- 5. "Thermodynamic and Transport Properties of Helium", by W. P. Wilson, Jr. for Electric Boat Division of General Dynamics Corporation, January 1960.
- 6. "Thermodynamic Properties of Nitrogen" Research Bulletin 18 by Institute of Gas Technology, October 1952.
- 7. "Flow of Fluids through Valves, Fittings and Pipe" Crane Technical Paper No. 410, Crane Company, 836 S. Michigan Avenue, Chicago, Illinois.

APPROVAL

TR-4-13-2-D

SPECIALIZED COST STUDY LAUNCH COMPLEX 39 PNEUMATIC SYSTEM

ORIGINATOR:

2	Tar	1/	13.	Loeb	10/3/	<u>63</u>
Mary	R T	ah				

Marx B. Loeb Mechanical Section

APPROVALS:

Carl D. Jumb 10/8/63

Carl D. Lamb Mechanical Section

Charles R. Minton Chief, Mechanical Section

Chester T. Wasileski

Chief, Propellant Systems Branch

Theodor A. Poppel

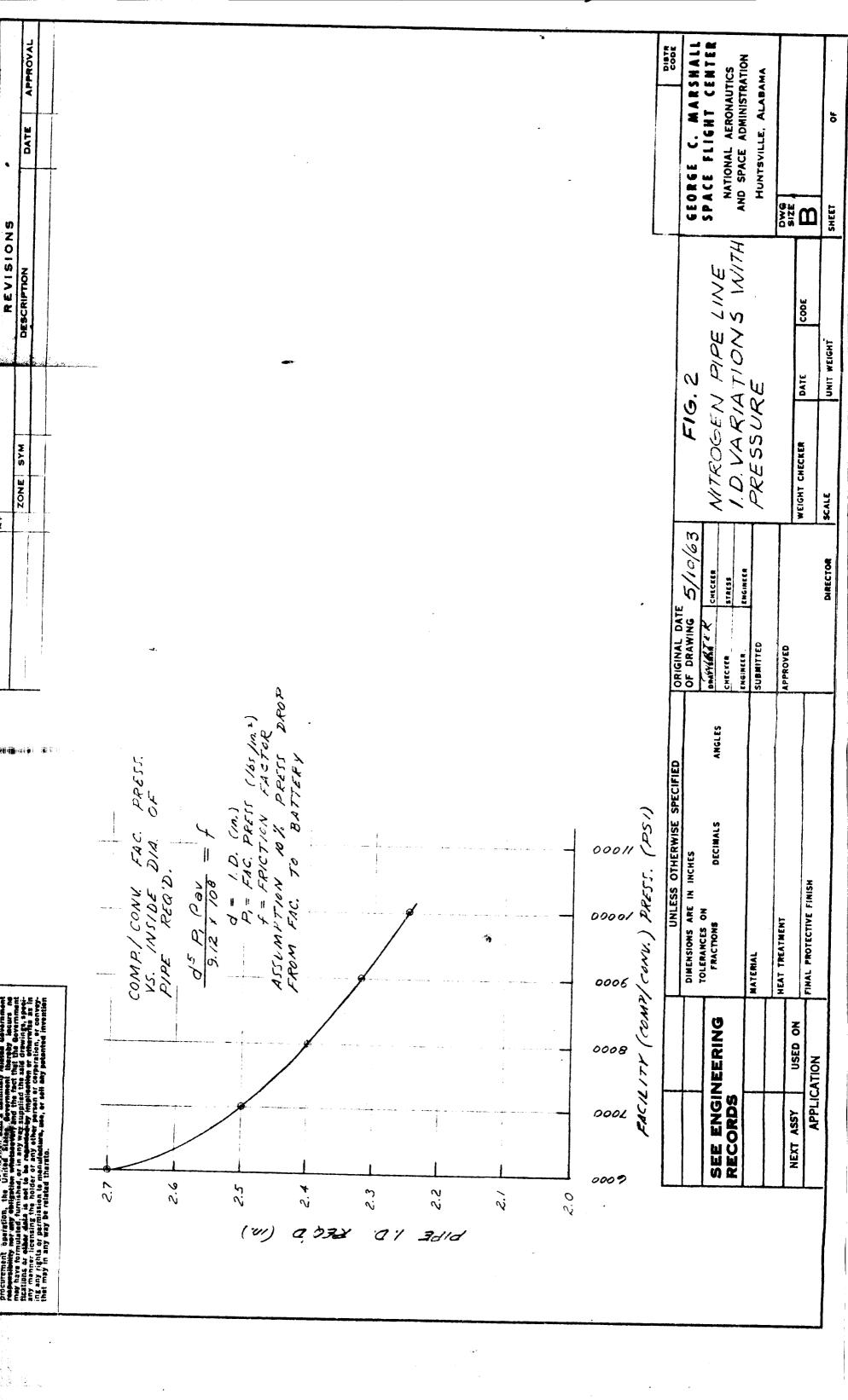
Director, Launch Support Equipment

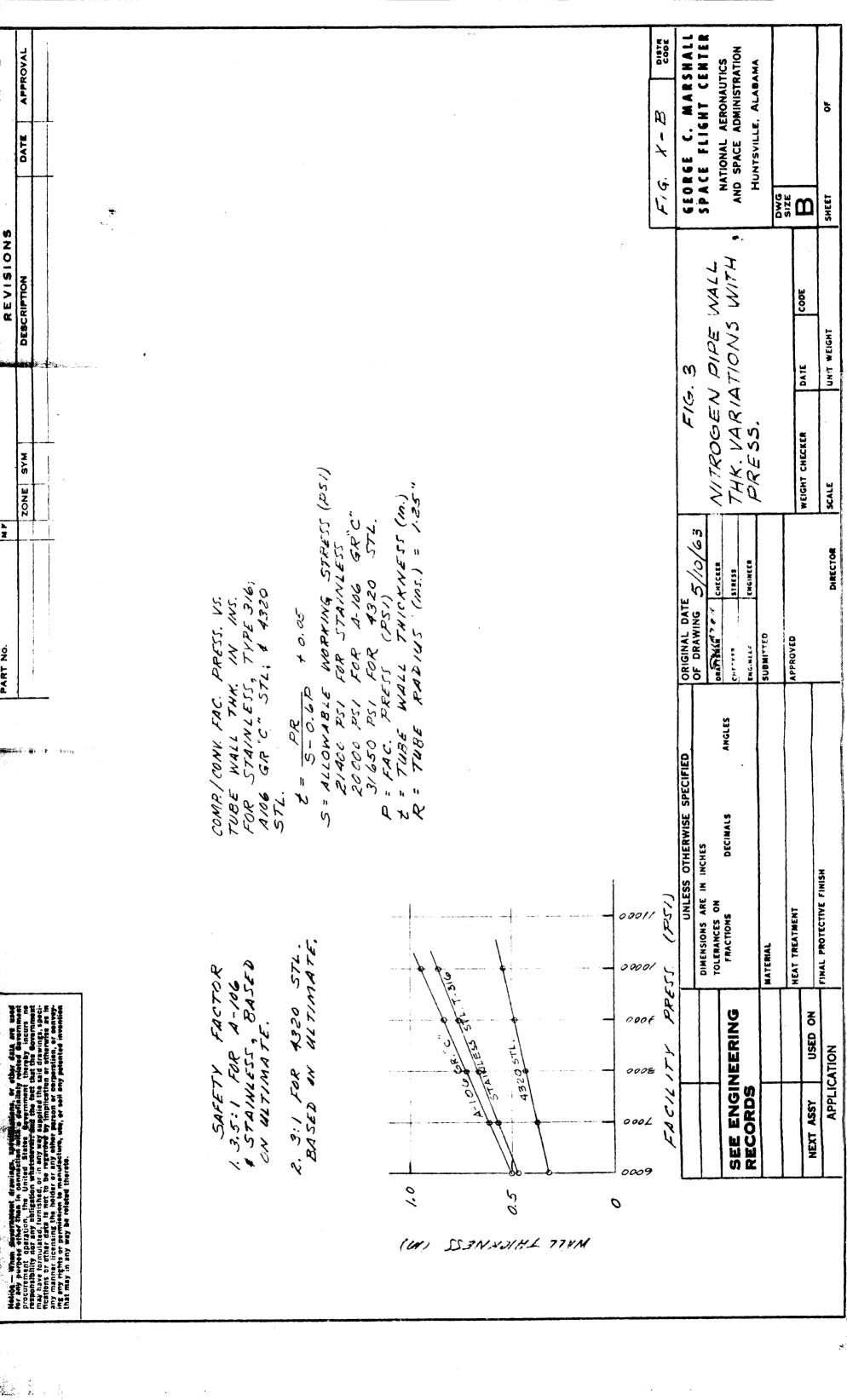
Engineering Division

	NOTES	BATTERY AND C/C FACILITY	10	. 4.		COLUMN 16 = COLUMN 10 + COLUMN 12	" 17= " 11+ " 13	<i>h' : + :: = 8 ::</i>	51 " + 11 " = 61 "	" 20 = COT. 16 + COL. 17 + COL. 18 + COL. 19	9.707 + 4.702 = 11.703	UAB COL. 10= COL. 7+COL.8+COL.9+COL.11	5+c>	- s/		011/509	5/6,560	052,330	438,405	084,4	05.2		GRAND TOTAL	/s 9014 025H s/	02	868 146 629 560'2 ECH' 282'9 2CH' 82H'	JSC, SET, 014, 411, 7 111, 416 B, 733, 756	7,203,030	184, 999	7,290,587 7,405,462 8,			
	ATT. TOTAL			=	62 823,362	862,514	05/206 05	22 944, 422		134 1161,134		A- COUNTRY PIPING TO	5500' 22" (GHZ) 5500 1"1.D. (GHC)	s 4106 s,	5/	3/0'5/8	332,200	320,980	310,035	135 299,090 414,	275 084,285 37Z	₩.	TOTAL COST VAR	18 001 A C	61	1,168,377	1, 194, 714	1 051,522,1	1 254,457	1,302,193	1, 443, 614 1,		
545C)	TESTING TOTAL BATT.		\overline{a}		120,000 1,645,862		050,426, 000,021		2018181 000 021	1,861	PIPING COSTS					Sh5'808 058'525'	1,643,600 297,825	105	256	800	L'222 056,481,1	FOR THREE PADS	PADC TO	028h 5/s		2,748,712 1,126,907	2,506,114 1,160,339	049,4610	418.339,374	2,321,903	1,345,884	666 81	•
O NAT OMON / NOO	· •		COST (#) COST (#)	7 @ 8	540,000 162,500		540,000 162,500	S40,000 150,000	540,000 150,000	540,000 150,000	TRANSMISSION	X-COUNTRY PIPING TO	17,500 22"1.0 (GN2) 17,000 1"1.0 (GHE)	320 A106	71	5.825 1,097,775	000'50' 529'246	930,650 1,021,130	068'986 200'026	059'156 56,650	867,825 898,800	CUMULATED TOTALS	TOTAL COST PA	4320 A106	<i>8</i> 0	1,789,187 1,921,137	1,810,139 1,919,514	082,800 1,923,280	218'0561 184'498	851,456, 878,358	456,820,2 856,820,5	1 SPAPE (2) 166,	
BATTERY & YOUN	repy		STORAGE(FT) COSTS (#) COST		156,474 541	163,760 540		181, 222 540			COUNTRY	PAD B	1"1.0.(GHC)	5/5	•	1,265,230 965	1.080,080	666,690	916 665	866,640	778,550	PAD AND	PAD B T	s/s 43		265'880'2	465'246'1	1,868,840	1,861,087	1,869,743 1,	1,939,684	CONVERTERS +	
PART.	TOTAL REOD PAD		COST (#) STORAGE(F	T U	2011 888 1706	H102 HSL'869	9173 986 5419	•••	809,676 3121	971,764 4427	55020	X-COUNTRY PIPING TO	11500'12 (GN2) 11,500	320 A 106	51	634,685 721,395		011,570 671,140	604, 612 648, 255	597,655 625,370	0,585 590,640	UNIT COST PER	TOTAL COST	320 A106	71	1,458,047 1,544,757	485,239 1,556,974	513,720 1,573,290	1,549,034 1,592,677	1,600,758 1,628,473	419 1,751,74	0000A. \$ 5 LM.	
	トルク	VESSEL	COST (#/H) COS	m	~	131 698	21 411		200	83 971	And the second s	-		5/s 43		1,430,260	1,220,960	0862501	1,036,230	979,680			∢	s/s 4 3		3,076,122	166'506'2	2,817,430 1	259'066'2	2,792,783	2,741,234 1,	1 SPARE @ \$28000 6A	,
	STORAGE RECMTS (FI*)	AVAIL	#GN. #GHe	2	1286 3220	1470 3864	1735 4664	6825 1161	8419 4112	1918 1462		X - COUNTRY PIPING	13,000 22" 1.D.(GNZ)13,000 1"10. (GHE)	4320 A106	21	717,470 B15,490		691,340 758,680					TOTAL COST PAD	4320 A106	16	258 1942 288 298'2			252,487, 2,487,232	4000 2,488,713 2,520,043		COMPRESSORS +	
	BATTERY ST		RANGE, (PSI) #6		10,000 - 4000		8000 - 1000	7500 - 4000	7000- 4000	(0000- 1000)		BATTERY		RANGE (PSI) 4		10,800 - 4,000	0004-	8000 - 4000	1500 - 4000	1000 - 4000	0000 - 1600		BATTERY	PRESS. 4	RANGE (PSI)	10,000 - 4000 2,3	9000 - 4000 Z,3	8000- 4000	7500 - 4000 2,	7000- 4000 2,	6000 - 4000 Z,	(A) 4 HELIUM	

	UNLESS	UNLESS OTHERWISE SPECIFIED	ORIGINAL DATE		LIVIDORN J JUNE 1
	DIMENSIONS ARE IN INCHES	ICHES.	OF DRAWING 10 MAT 6		CLONGE C. BANGAREL
	TOLERANCES ON		DRAFTSMAN AB CHECKER	·)	STACE TEIGHT CENTER
SEE ENGINEERING	FRACTIONS	DECIMALS ANGLES	CHECKER	HANKS HOO SHINGANOS	NATIONAL AERONAUTICS
RECORDS			ENGINEER MY	_	AND STACE ADMINISTRATION
	MATERIAL A//A		SUBMITTED	TNEUMATIC SYSIEMS	HUNTSVILLE, ALABAMA
				COST COMPAYISONS	DWG
	HEAT TREATMENT		APPROVED		SIZE
NEXT ASSY USED ON	A//A			WEIGHT CHECKER DATE CODE	~
	FINAL PROTECTIVE FINISH	X			
APPLICATION	4//		001010		

.





APPROVAL GEORGE C. MARSHALL SPACE FLIGHT CENTER CODE AND SPACE ADMINISTRATION NATIONAL AERONAUTICS HUNTSVILLE, ALABAMA DATE M SE SHEET REVISIONS HELILIM PIPE LINE 1.D. DESCRIPTION VARIATIONS WITH CODE UNIT WEIGHT F16. 4 DATE PRESSUR WEIGHT CHECKER ZONE SYM PRE 55. SCALE FAC. PRESS E. : 10 % FAC. OF DRAWING 5/10/6 P. : FAC PRESS DIRECTOR 114. CHECKER ENGINEER f = FRICTION STRESS DSSUMPTION: DROF FROM A BATTERY d = 1.0. (11.) ds P, Par 1.36 x 10 FEO 'D. COMP. / CCNV 3015W .SN PART NO SUBMITTED APPROVED DELETSHAN CHECKER ENGINELX ANGLES UNLESS OTHERWISE SPECIFIED PRESS. (251) DECIMALS DIMENSIONS ARE IN INCHES 0006 FINAL PROTECTIVE FINISH TOLERANCES ON FRACTIONS HEAT TREATMENT MATERIAL 00.78 vertex — When Government drawings, specifications, or other data are used for any gurpose other than in connection with additively helded Government proculement operation, the United States devernment thereby incurs no max have formulated fourished, or in any way supplied the set that the Government fications or other data is not to be regarded by implication or other data is not to be regarded by implication or otherwise as any manner licensing the holder or any other person or cerporation, or converting any rights or permission to manufacture, use, or sell any patential invention. SEE ENGINEERING RECORDS USED ON FAC 0002 APPLICATION **NEXT ASSY** 0009 0% 25 1.05 1.10 0.30 Ö. ·Q 1 Pald

